

**Orchid Chemicals & Pharmaceuticals
Ltd.,**

COMPANY PROFILE IN BRIEF

- **Manufacturer of bulk Cephalosporin range of products (antibiotics), Intermediates and Neutraceuticals with two sophisticated manufacturing facilities in India (one at Alathur near Chennai and the other at Aurangabad)**
- **Our Alathur facility has a work force of about 1200 and a turnover of Rs.648 crores**
- **Largest manufacturer of Cephalosporin products in India and one among the top five in the world**
- **100% EOU with ISO 9000, ISO 14000, US-FDA, TGA EDQM, MHRA certifications**



NATURE OF MANUFACTURING

- **Cephalosporin manufacturing is based on low temperature technology upto -70°C and beyond**
- **Approx. 4700 TR equivalent of refrigeration systems at various temperatures (+7,0,-10, -25, -30, -40 & -70deg.C)**
- **Steam generation of 22 Tons/ Hour**
- **Energy cost is approx. 6.2 % of the turnover**
- **Zero discharge by Evaporation, Ultra Filtration & RO technology**
- **A typical manufacturing process stream is as under:**

**Reactors - Centrifuging - Drying - Powder Processing - Cold Storage –
Despatch**

ENERGY SCENARIO

➤ **Electrical power**

CPP 10.56 MW (3.38 x 2nos. + 3.8 x 1no. FO Gensets)

110 KV TNEB supply is in service as a prime source. Due to TNEB realisation the plant demand has come down to 9.5 MVA against 10.5 MVA when operated on CPP due to improvement in p.f

Wheeling from gas generated units from Ramnad is in force

➤ **Steam**

550 Tons per day

4 Nos. of FO fired boilers ,3 Nos.of WHRBs

➤ **Fuel bill - approx. Rs.40 crores per annum**

(50% for Utility, 20% for ETP and 30% for process)

Summary of Encon Projects 2004 - 07

Sl. no.	Year	Total No.of Projects	Savings / annum (Rs.in Lacs)
1	2004 - 05	4	138.1
2	2005 - 06	18	276.7
3	2006 - 07	26	466.4
4	Target for 2007 - 08	28	700.0



Summary of ENCON activities for the year 2004 -07

Sl.no.	Activities	Savings/Annum achieved in Lakhs
1	Innovative projects	315.57
2	Continuous improvement projects	565.73
3	Specific energy consumption reduction from 42.99 to 39.92	7.14%
4	Renewable energy sources	
	Wind	208.1
	Solar thermal	20.8
	Biomass	110.8



**List of Projects with
cost Benefits
(2004-05 & 2005-06)**

List of ENCON Projects with cost Benefits 2004 – 05

No.of Projects :- 4 Total Savings :- 138.11 Lacs

S.No.	Title of Encon Projects	Energy saved/annum		Savings/ annum
		Electrical (Units)	Thermal (FO in KL)	(Rs.in lakhs)
1	In MPSR chiller the load on +10 refrigeration system was shifted to CT. The load on CT was shifted to air cooled radiators	1800000	0	47.52
2	Load on -65 refrigeration system was shifted to -70 system (The KW per TR in the former was higher)	1050000	0	27.72
3	In Solvent Recovery continuous distillation the feed tray location was optimised to have more stripping section resulting in the "nil" reflux for a given purity	560000	168	30.50
4	In 16 TPH boiler the old centrifugal conventional burners have been replaced by the new Dunphy co-axial ratiotronic micro-processor controlled burner, which could trim the excess oxygen levels closer to 1.2% (the excess air required for combustion got reduced by 7%)	0	346	32.37
	TOTAL			138.11

List of ENCON Projects with cost Benefits 2005 – 06

No.of Projects :- 18 Total Savings :- 276.7 Lacs

S. no	Title of Energy project 2005 – 06	Energy saved / annum		Savings / annum (Rs. in Lacs)
		Electrical in Units	Thermal FO in KL	
1	Reduction of boiler flue gas to 150 deg. C. Hence to prevent corrosion, boiler was designed with Feed water heating coil inside the boiler to increase the feed water temperature.Fuel steam ratio 15.4	0	7842.50	96.30
2	Replaced vapour absorption system with water cooled energy efficient centrifugal compression system at utility-1	0	379.35	46.30
3	Bifurcation of HP condensate to Boiler and LP condensate to Ecology	0	13.80	1.50
4	Operating the waste heat recovery boiler at low pressure and thereby 500 kg/hr steam generation increased	0	270.96	43.00
5	In Utility 40TR and 102TR systems, evaporative condenser fan pumps were interlocked with compressor	30657		1.50

List of ENCON Projects with cost Benefits 2005 - 06

S.no.	Title of Energy project 2005 – 06	Energy saved / annum		Savings / annum (Rs.in Lacs)
		Electrical in Units	Thermal FO in KL	
6	Additional pump, operation stopped by relocating the distillation column condenser from higher level to lower level	50000	0	1.70
7	Lube oil economizer lined up in the lube oil line to increase the engine return oil temperature to 75 deg from 65 deg. C	170000	0	6.20
8	By continuously monitoring the flow pattern and rectifying the leakages. Installing pressure reducing valves for low pressure application.	670000	0	23.20
9	Optimization of cooling tower usage by interconnecting the cooling tower and pumps delivery lines and stopping one cooling tower pump and fan	440000	0	15.20

List of ENCON Projects with cost Benefits 2005 - 06

S.n o.	Title of Energy project 2005 – 06	Energy saved / annum		Savings / annum (Rs. in Lacs)
		Electrical in Units	Thermal FO in KL	
10	Segregation of cooling tower pumps based on different head level	160000	0	5.50
11	Ecology incinerator system I.D. Fan stopped by interconnecting evaporator & Scrubber vent	180000	0	6.20
12	Provided Desuper heater for –40 deg.C40TR Refrigeration system	100000	0	3.40
13	Interlocking of centrifuge Hydraulic system motor such a way that it will run only when scrapping and door opening of centrifuges. Done for three centrifuges).	16826	0	0.70
14	Higher head pump replaced with lower head pump in 0 deg C refrigeration system	130000	0	4.50

List of ENCON Projects with cost Benefits 2005 - 06

S.no.	Title of Energy project 2005 – 06	Energy saved / annum		Savings / annum (Rs. in Lacs)
		Electrical in Units	Thermal FO in KL	
15	Primary pump operation eliminated in refrigeration system	260000	0	9.00
16	Reduction in lamp wattage by converting 160 ML lamp to 3x 18 w CFL lamps considering the required illumination level (90 fittings converted)	40000	0	1.40
17	Pumps impeller trimmed based on the load requirement.	205495	0	6.90
18	Optimizing the compressor usage by adjusting the compressor tripping set point from 0 deg.C to 5 deg.C.	100960	0	4.20
Total				276.7



List of Projects with Cost benefits (2006-07)


ENCON ACTIVITIES 2006-07 AN OVERVIEW

S.No	Activities	Annual Energy Savings				Total Rs.Lacs
		THERMAL		ELECTRICAL		
		FO(KL)	Rs. lacs	Units	Rs. lacs	
1	Continuous improvement Projects	206.9	31.0	7441770	331.6	362.6
2	Innovative Projects	326.3	52.2	1248230	54.9	103.8
TOTAL SAVINGS						466.4

List of Continuous improvement ENCON Projects :

No Investment

S.no.	Title of Continuous improvement ENCON project 2006 - 07	Energy saved / annum		Savings / annum (Rs. in Lacs)
		Electrical in Units	Thermal FO in KL	
1	Optimizing the chilling plant pumps operation by regulating flow rate.	1139530	0	50.58
2	Auto operation of chilling plants	354050	0	15.72
3	In PH-18 Non critical area heat load reduced by eliminating heating and cooling system	0	84.00	12.60
4	Elimination of furnace oil heating in storage tank	54750	0	2.43
5	Optimizing the refrigeration usage in process area by increasing the chiller set points without affecting the process	803000	0	35.65
6	Optimising the refrigeration accessories operation by interlocking	60225	0	2.67

List of Continuous improvement ENCON Projects :

S.no.	Title of Continuous improvement ENCON project 2006 - 07	Energy saved / annum		Savings / annum (Rs. in Lacs)
		Electrical in Units	Thermal FO in KL	
7	LP steam from evaporator given to Phase-19 and HP steam from boiler isolated	0	122.94	18.44
8	Desuperheater installed in -70 VGC	20440	0	0.91
9	Optimization of efficient centrifugal chiller operation	876000	0	38.89
10	Installation of inverter for Utility-1,2&3 – 10 deg sec pump	97455	0	4.32

List of Continuous improvement ENCON Projects :

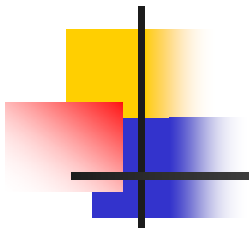
S.no.	Title of Continuous improvement ENCON project 2006 - 07	Energy saved / annum		Savings / annum (Rs. in Lacs)
		Electrical in Units	Thermal FO in KL	
11	Optimization of chilling plant , cooling towers accessories,operation tower	156950	0	8.9
12	B-1206 Scrubber blower motor 70HP is replaced with 45HP	87600	0	3.89
13	Converting -10°C brine circulation by chilled water for powder process AHUs	337625	0	14.99
14	Elimination of primary pump in -10/ 30TR and 50TR systems	205130	0	9.11
15	Effective utilisation of cooling tower by interconnecting near by cooling tower	855560	0	37.98

List of Continuous improvement ENCON Projects :

S.n o.	Title of Continuous improvement ENCON project 2006 - 07	Energy saved / annum		Savings / annum (Rs. in Lacs)
		Electrical in Units	Thermal FO in KL	
16	Liquid nitrogen connection and bifurcation of LP & HP nitrogen ,air circuits.	1462920	0	64.95
17	Installation of economizer to reduce the power consumption by improving the chiller efficiency –25/102 TR	78840	0	3.5
18	In PH-19 AHU-1901 no. of air changes reduced.	13870	0	0.62
19	In –12/100TR plant by increasing the RPM of the evaporative condenser blower discharge pressure was reduced	176660	0	7.84
20	Phase-25 plant + 7 Chilled water 30TR load shifted from MPSR air cooled chiller to +7 water cooled chiller in Utility-1	146000	0	6.48

List of Continuous improvement ENCON Projects :

S.n o.	Title of Continuous improvement ENCON project 2006 - 07	Energy saved / annum		Savings / annum (Rs. in Lacs)
		Electrical in Units	Thermal FO in KL	
21	Installation of inverter for -10°C secondary pump in Utility-3 , -10°C secondary pump in Utility-1	97455	0	4.32
22	Conversion of 160W ML (Mercury Lamp) fittings to CFL (Compact Fluorescent Lamp) 54 Watts	197730	0	8.78
23	Elimination of primary pump in -10/30TR1 & 2, -10/50TR 1 & 2	205130	0	9.11
Total				362.6



Innovative Projects implemented in 2006-07

List of Innovative ENCON Projects : 2006 - 07

S.n o.	Title of Innovative ENCON project 2006 - 07	Energy saved / annum		Savings / annum (Rs. in Lacs)
		Electrical Units	Thermal FO in KL	
1	Using Calorimetry for process reaction	992730	-	43.5
2	In PH-18 Hot water coming out of AHU is diverted to WFI Cooling	255500	222.84	44.76
3	Optimization of Distillation column operation Aspen Software	0	103.47	15.51
Total				103.8

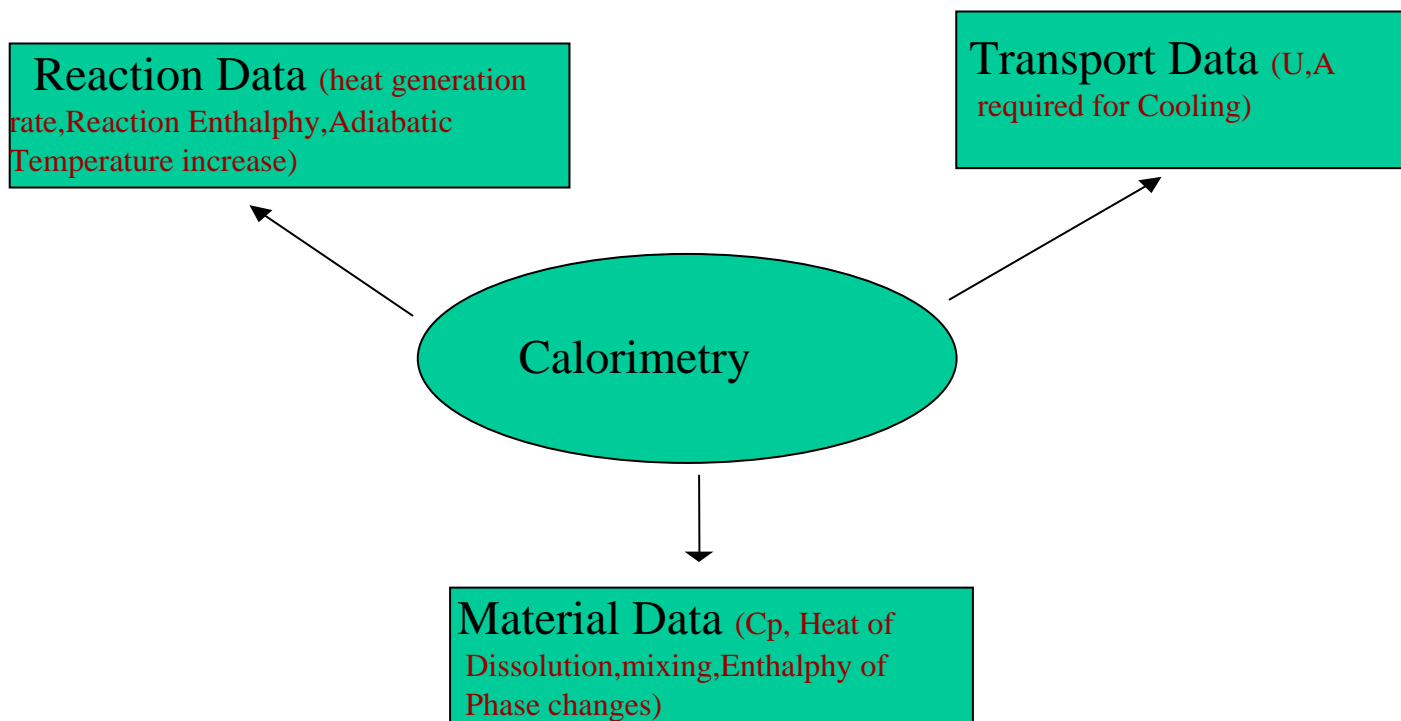


Innovative Projects implemented in 2006 - 07

**1.Using reaction calorimetry for
optimising the energy requirement
In the Chemical Reactions**

Using reaction calorimetry for Chemical Process

Information that could be generated through Reaction Calorimetry

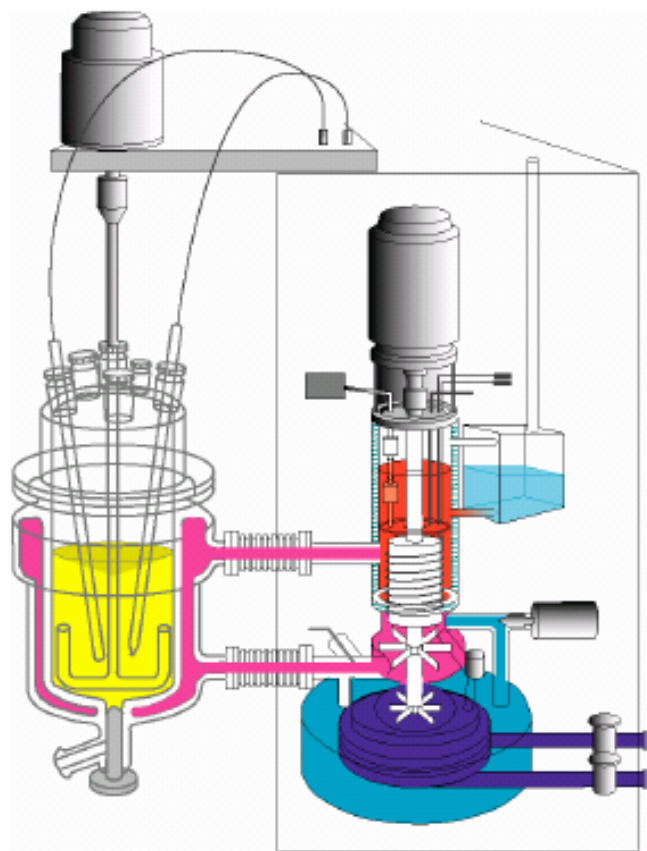


Using reaction calorimetry for Chemical Process

REACTION CALORIMETER---METTLER, RC1e



Equipment Details: RC1e's Thermostat system



Complete instrument family
covering widest application ranges:

- ◆ temperatures: - 90 °C ... + 300 °C
- ◆ heat flow at reactor: ± 350 W/kg
- ◆ temperature control modes:
isothermal-, isoperibolic-,
adiabatic- and distillation-mode
with high heating and cooling
rates
- ◆ sophisticated safety system



Using reaction calorimetry for Chemical Process

Example

- a. Consider a process (Temp desired = 0 ± 5 Deg C) that is exothermic in nature with a high adiabatic temperature rise (40 Deg C)
- b. The heat of reaction from calorimeter gives the exact reason for the adiabatic temperature rise ,whether due to
 - 1, Reaction
 - 2, Reagent addition
- c. Based on the heat release rate and the type , we can decide the process temperature and the utility temperature that is required



Using reaction calorimetry for Chemical Process

- Exact utility type/temperature required for the process

Present Process	Recommended Process
<ul style="list-style-type: none"> •Process temperature :-40 Deg •Reagent addition : dumping •Dosing Reagent Temp: 5 Deg c •Utility temperature : -70 Deg C •Total Process Time : 4 hrs <p><i>Utility load has to overcome both heat of reaction and heat of dosing and dosing heat is dominating in this case</i></p>	<ul style="list-style-type: none"> •Process temperature :0 Deg C •Reagent addition : Controlled •Dosing Reagent Temp: 0 Deg c •Utility temperature : -10 Deg C •Total Process Time : 2 hrs <p><i>Utility to overcome heat of reaction only and dosing reagent is to be reduced to 0 Deg C</i></p>

Using reaction calorimetry for Chemical Process

- Optimal Flow rate of the utility required.
Minimum flow rate of the utility required for the process of interest could be calculated based on the rate of heat that is released/ absorbed by the process
- Optimal Surface area for heat transfer controlled processes
there-by selection of right reaction vessels.

*Utility costs **14.56 Lacs/Annum** are drastically reduced by making using of higher temperature brine*



Innovative Projects implemented in 2006-07

**2. Optimum utilisation of Energy
in Water for injection system
(WFI) and Air Handling Units
(AHU)**

(Refer Schematic diagrams on the following pages)



Optimum utilisation of Energy in Water for injection system (WFI) and Air Handling Units (AHU)

✦ **Existing Practice** : Steam was used to heat the dehumidified air in AHU and 0°C brine is used to cool the pure steam generated in WFI system

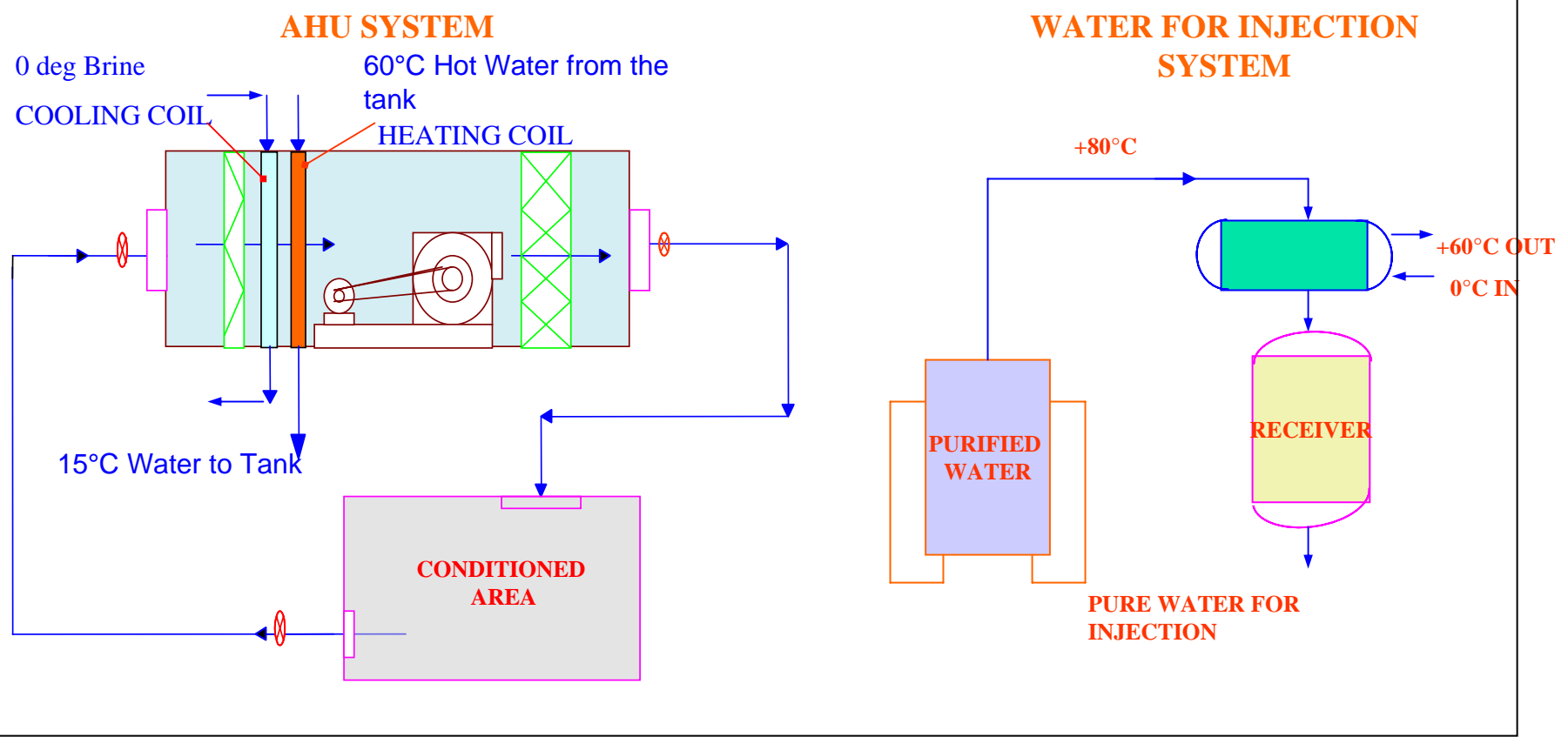
✦ **Modified Practice** : Water is being used to cool the pure steam generator and hot water which is coming out from the WFI is circulated to AHU heating coil

✦ **Investment** : Rs.1 Lacs

✦ **Savings Achieved** : Rs.44.7 Lacs/Annum

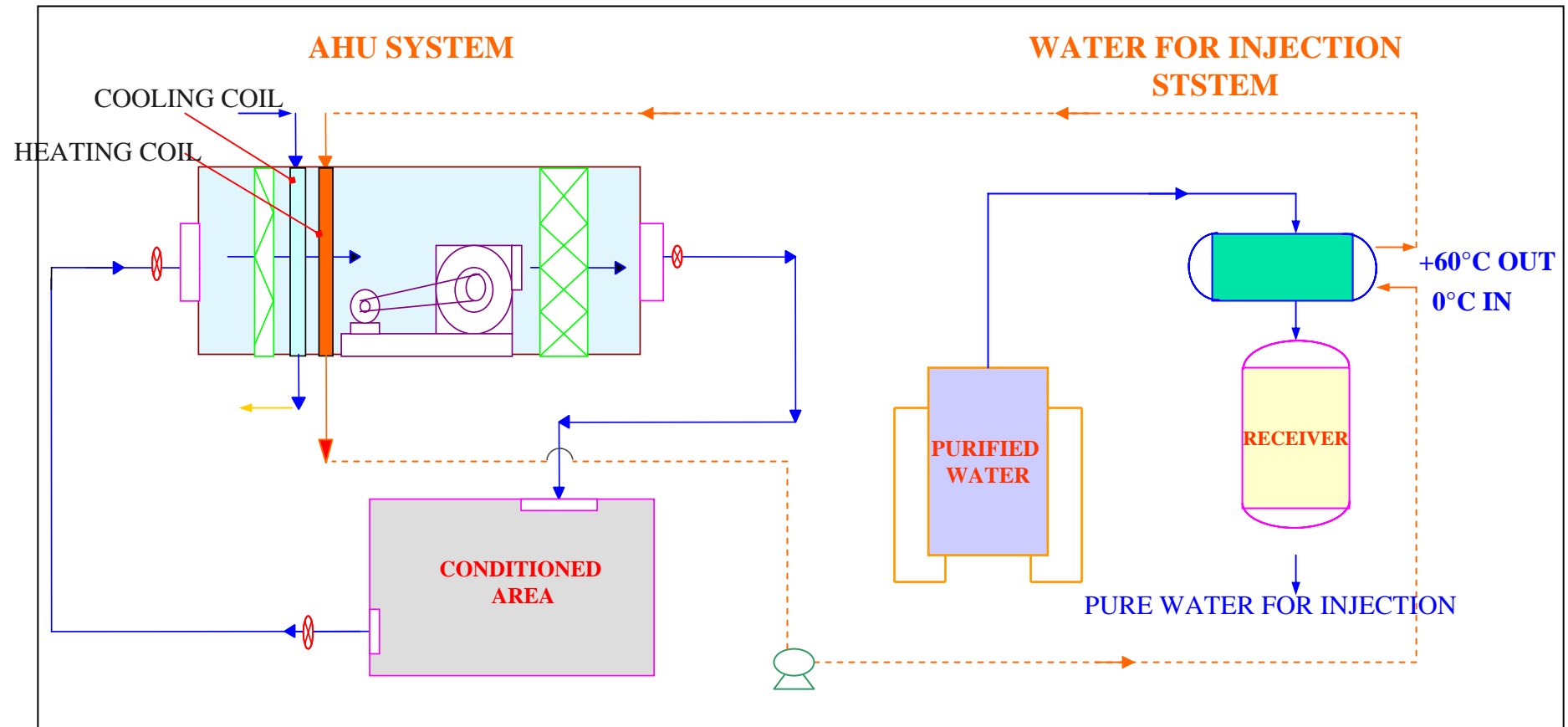
Optimum utilisation of Energy in Water for injection system (WFI) and Air Handling Units (AHU)

Existing System



Optimum utilisation of Energy in Water for injection system (WFI) and Air Handling Units (AHU)

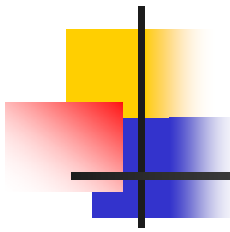
Modified System





Innovative Projects implemented in 2006-07

**3. Optimization of distillation
column operation using Aspen
Software (Simulation Technology)**



Optimization of distillation column operation using Aspen Software (Simulation Technology)

Features of Aspen Software

- The column operations can be optimized based on energy, impurities, etc. and various constraints like condenser & reboiler duty.
- Detailed heat and mass balance Can be calculated for all the unit operations like heater, cooler, condenser and reboiler load for distillation column.
- For reducing energy various scenarios can be created using either sensitivity analysis e.g. change of column pressure, reflux ratio, feed tray location, etc.
- Using batch reactor model, we can calculate the optimum reaction time & temperature in a batch reactor

Optimization of distillation column operation using Aspen Software (Simulation Technology)

Example

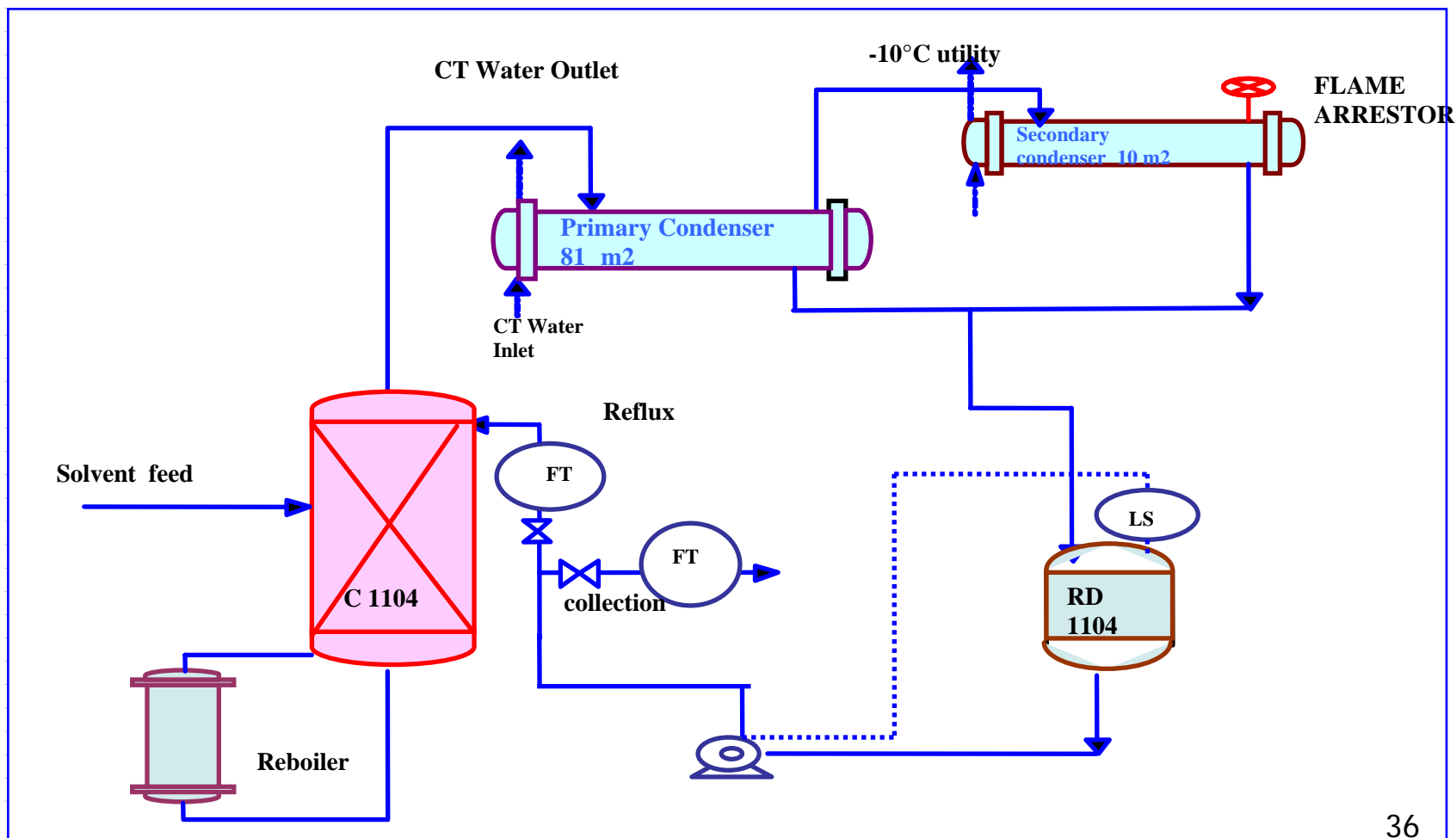
✦ **Existing Practice** :Reflux ratio was maintained 8 to separate Ethyl Acetate (EA) & Tetra Hydro Furan(THF) from EA+THF mixture

✦ **Modified Practice** :Reflux ratio was reduced to 5 from 8 to separate EA & THF from EA+THF mixture without affecting the quality

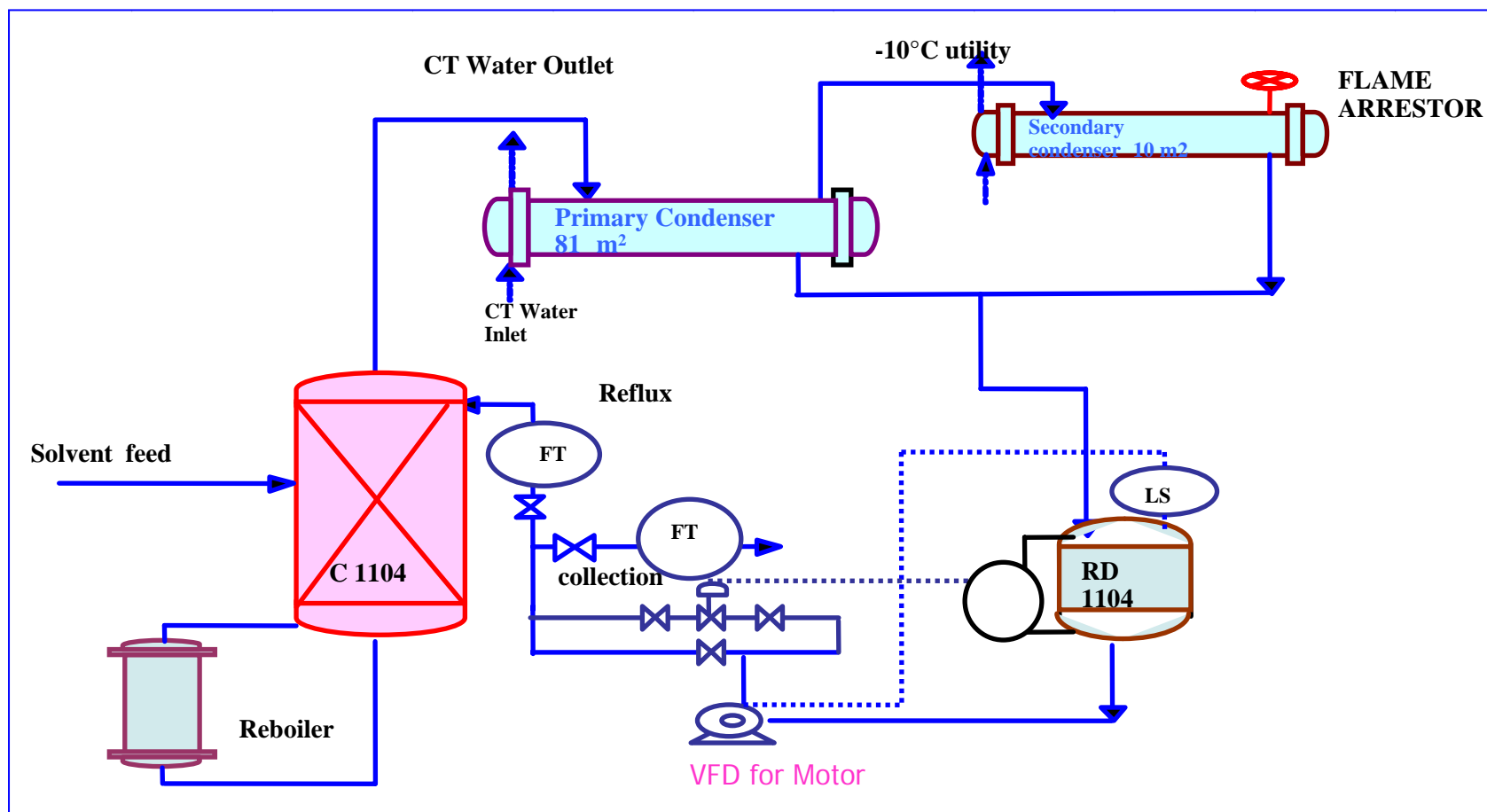
✦ **Investment** : Rs.2 Lacs

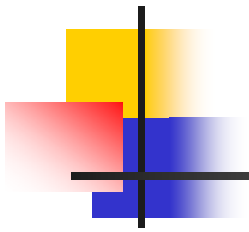
✦ **Savings Expected** : Rs.17 Lacs/Annum (In terms of steam reduction)

Distillation setup before modification



Distillation setup after modification

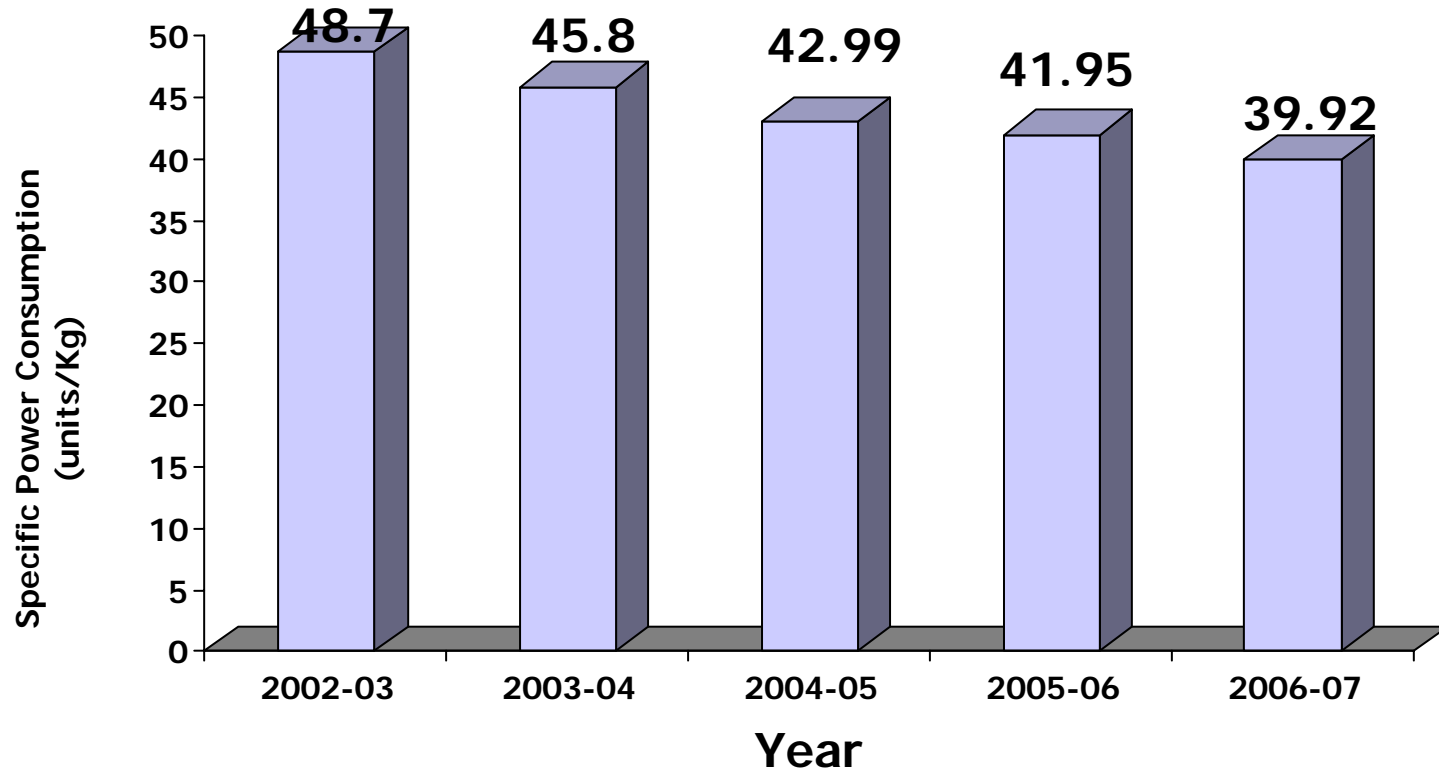




**Sustainability in
reduction of
Specific energy
consumption norms**

Sustainability in reduction of Specific energy consumption norms Power

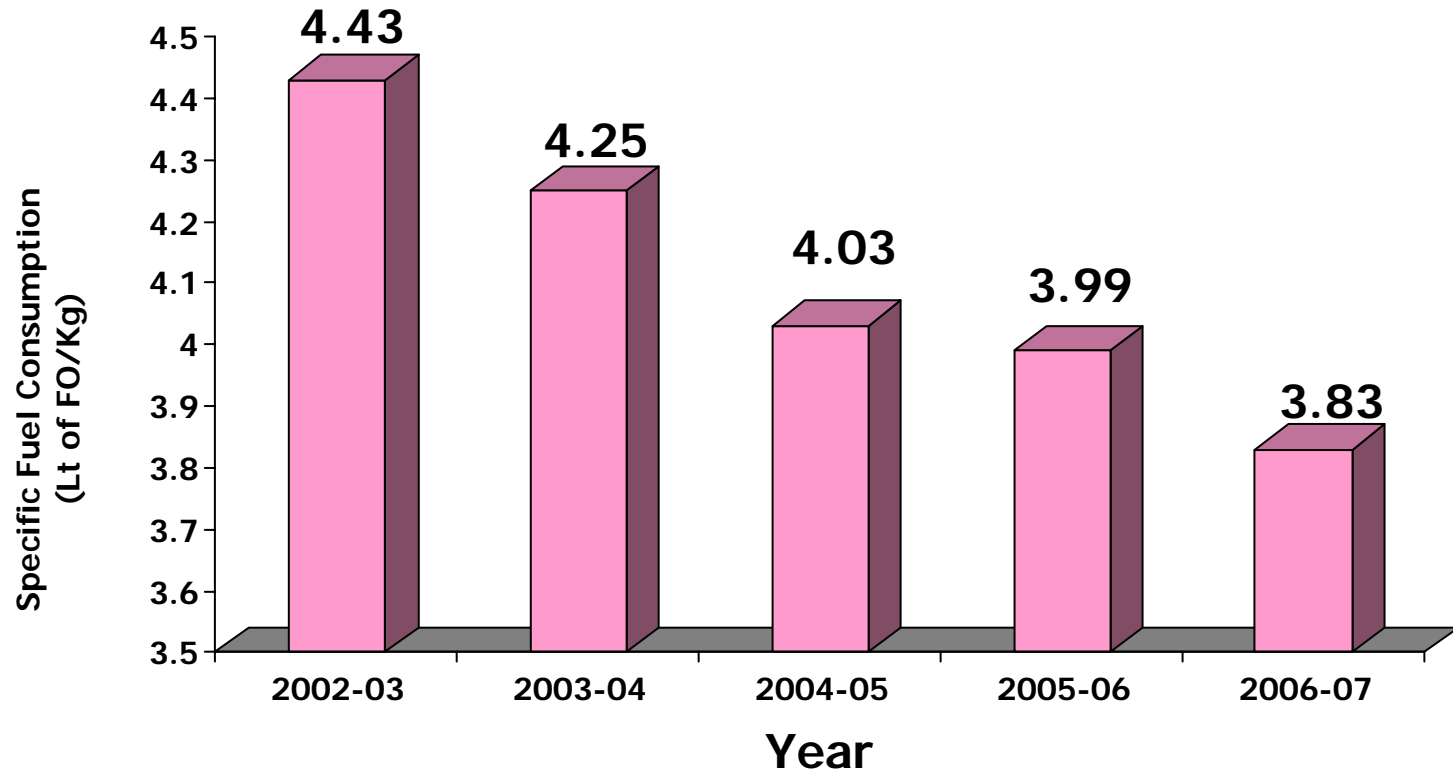
Reduction in Specific Power Consumption (Units/kg)



Sustainability in reduction of Specific energy consumption norms

Thermal

Reduction in Specific Fuel Consumption (Litres of FO/kg)





Renewable Energy and Environmental projects

Renewable Energy and Environmental projects

1. Solar Evaporation



The rate of evaporation = 3 mm per day

Equivalent Fuel Savings = 75 KL per annum

Savings about = Rs.10Lacs per annum

2. Utilisation of Waste

Composting of Bio-Sludge

- Bio-Sludge generation- -360 tons per annum
- Equivalent Fuel Savings = 349 KL
- Savings about = Rs.45.0Lacs per annum

Composting of Effluent Treatment Plant Bio-Sludge (Dynamic Pile Process)



Alternative to Incineration



3. Energy conservation by conserving water

- **Orchid, being a 'Zero Discharge Unit', adds value to water by 100% recycling**
- **Saving 150000 KL of water/ annum by recovering water from effluent using\ UF and RO**
- **By using air cooled heat transfer equipment, Water evaporation loss of 75000 KL/year is avoided**
- **A major part of CT make up water is obtained from:
Defrost water, container wash water, AHU humid water, water ring vacuum pump expel water, hot water tank, overflows, reactor jacket draining etc.**
- **Providing orifices before the water usage points**

All the above resulted in the reduction of specific water consumption

MONITORING AND REPORTING SYSTEM

Daily Steam & Power consumption at various user ends are monitored, recorded and reported on daily basis to the respective user departments and displayed in the notice board.

Systemwise energy meter provided and reported on daily basis.

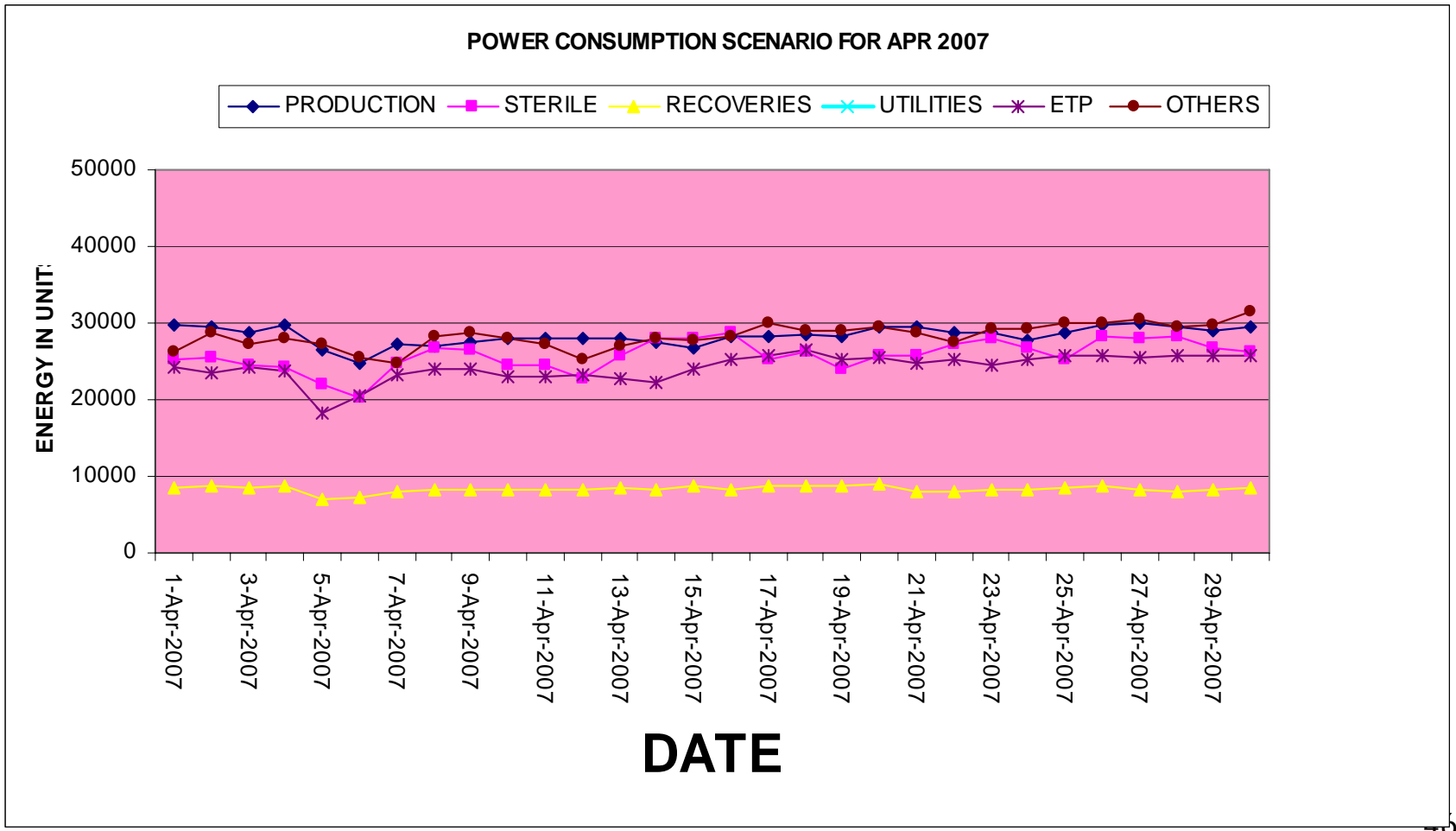
Shiftwise 'A' category power consumption reported and monitored.

On line oxygen analyser to operate the nitrogen plant with optimum air consumption.

Sample reporting format is as follows:

S.No.	Date	Product name	Qty.	Power units	Fuel (lit)	SPC	SFC
1.	30.07.06	Cephalexin	2000 kgs	83900	7980	41.95	3.99

Department wise Power Trend



Daily Power Report

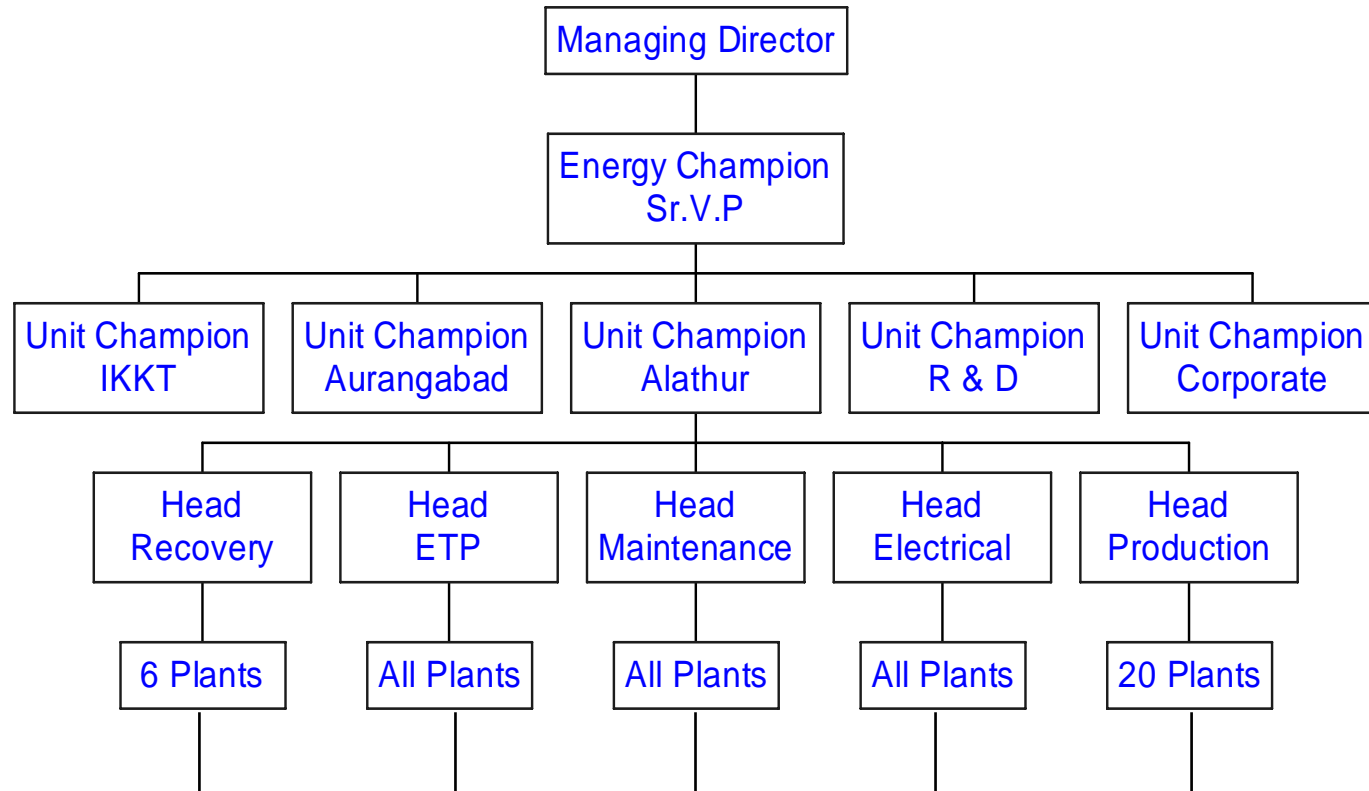
"Information Motivates, Empowers shift operators !"

16.07.2007

	Shift-In-Charge	Utility-1		Utility-2	
		kwh	Operator	kwh	Operator
A	J. Krishnamoorthy	5861	Venkatesh/Balan	9834	Venkatesan
B	K. Kannadasan	6239	Karthic/Balan	10156	Madhan
C	Venkateswarayadev	5659	Babu/Elumalai	10106	SAGADEVAN
TOTAL			17759		30096

PLANT	EQUIPMENT NAME	A/SHIFT - 05.00 HRS			B/SHIFT - 21.00HRS		
		INITIAL	FINAL	DIFF	INITIAL	FINAL	DIFF
UTILITY-1 REFRIGERATION	-10/110 TR	61429	62692	1263	62692	63940	1248
	-10/30TR-1	266900	267300	400	267300	267600	300
	-10/30TR-2	201300	201700	400	201700	202200	500
	-10/50TR-1	271300	271700	400	271700	272100	400
	-10/50TR-2	384300	384600	300	384600	384800	200
	TOTAL		2763			2648	
	-25/102 TR	0	0	0	0	0	0
	-30/10TR HS	11690	11800	110	11800	11920	120
	-30/10TR LS	0	0	0	0	0	0
	-30/20TR HS	33040	33160	120	33160	33190	30
	-30/20TR LS	21340	21400	60	21400	21470	70
	-40/40 TR	55418	56632	1214	56632	57933	1301
	-70 POWER		1504			1521	
	-70/'X' HS	282300	282300	0	282300	282400	100
	-70/'X' LS	189900	189900	0	189900	190000	100
	-70/'VGC' HS	55204	55324	120	55324	55673	349
	-70/'VGC' LS	17517	17591	74	17591	17812	221
	-70/ NEW HS	626100	626800	700	626800	627600	800
	-70/ NEW LS	479400	480100	700	480100	480600	500
	TOTAL		1594			2070	
TOTAL UTY-1		5861			6239		

ENCON ORGANOGRAM



Operating and Maintenance personnel at the shop floor



Role of Energy Manager

- **We have a Designated Energy Manger**
- **Two Energy Manager have been sponsored for energy management exam.**
- **Fortnightly review meetings are organized and once in a month review with MD**
- **The saving proposals are discussed in the Meeting**
- **The energy audits are conducted in every quarter**

Excellent Energy Efficient Unit – 2005-06



MOTHER TERESA AWARD – BEST CORPORATE CITIZEN 2000



ORCHID'S MODEL FOR SUSTAINABILITY

