

## **Issue # 1: June 2008**

### **IGEN – Thermal Power Plant Corner**

Estimation of savings due to control of de-super heater water spray

#### **Background:**

A 140 MW thermal power generating unit, operating at 110 MW, was found to having main steam flow of 390 Ton/hr (TPH) at 120 kg/cm<sup>2</sup>(g) pressure and 536°C temperature (enthalpy = 822.9 kCal/kg). To control the super heat temperature, 30 TPH of water spray at 128 kg/cm<sup>2</sup>(g) and 170°C (enthalpy = 173.4 kCal/kg) was used in the de-super heater. The other operating parameters/ assumptions of the generating unit are as under:

#### **Parameters/ Assumptions:**

- a) Main steam required at the above main steam pressure & temperature to generate 1 MW = 3.5 TPH.
- b) Specific coal consumption = 0.65 kg/kWh
- c) Coal GCV = 4,600 kCal/kg
- d) Landed coal cost = Rs. 1,800 per ton
- e) Expected steam consumption in the soot blowers after repair = 110 ton per day
- f) Average revenue realised = Rs. 2 per kWh generated
- g) Investment towards repairing of soot blowers = Rs. 4 crores
- h) Boiler efficiency = 80%
- i) Annual plant operating hours = 7000

#### **Proposal:**

The power plant plans to repair the existing steam soot blowers in order to improve the heat transfer within the boiler and to reduce the de-super heater water spray from 30 TPH to 7 TPH.

#### **Issue:**

What will be the energy and money saving potential if the above proposal is implemented by the power plant management?

Please send your solutions latest by 10<sup>th</sup> July 2008 to Mr. K. K. Chakarvarti,

Manager – Power Plant Component at [ppc@energymanagertraining.com](mailto:ppc@energymanagertraining.com)

All the best solutions received will be posted on the website latest by 17<sup>th</sup> July 2008 alongwith the names of the contributors.

**Solution:**

**Part – 1:**

Steam required for power generation

$$= 3.5 \text{ TPH} \times 110 \text{ kW}$$

$$= 385 \text{ TPH}$$

Main steam flow = 390 TPH

Steam used for soot blowing = 390 – 385 TPH

$$= 5 \text{ TPH}$$

$$= 120 \text{ TPD}$$

Steam consumption after repairing soot blower

$$= 110 \text{ TPD}$$

Steam savings = 120 – 110 TPD

$$= 10 \text{ TPD}$$

$$= 0.416 \text{ TPH}$$

Option – 1:

$$\text{Steam cost} = \frac{(822.9 - 173.4) \text{ kcal/kg} \times \text{Rs. } 1800/\text{T}}{0.8 \times 4600 \text{ kcal/kg}}$$

$$= \text{Rs. } 317.7 / \text{Ton}$$

Annual Savings = Rs. 317.7 / T x 7000 hrs x 0.416 TPH

$$= \text{Rs. } 9.25 \text{ Lakhs}$$

Option – 2:

The saved steam can be passed through turbine and can generate additional power

3.5 TPH steam generates 1 MW, therefore 0.416 TPH steam generates

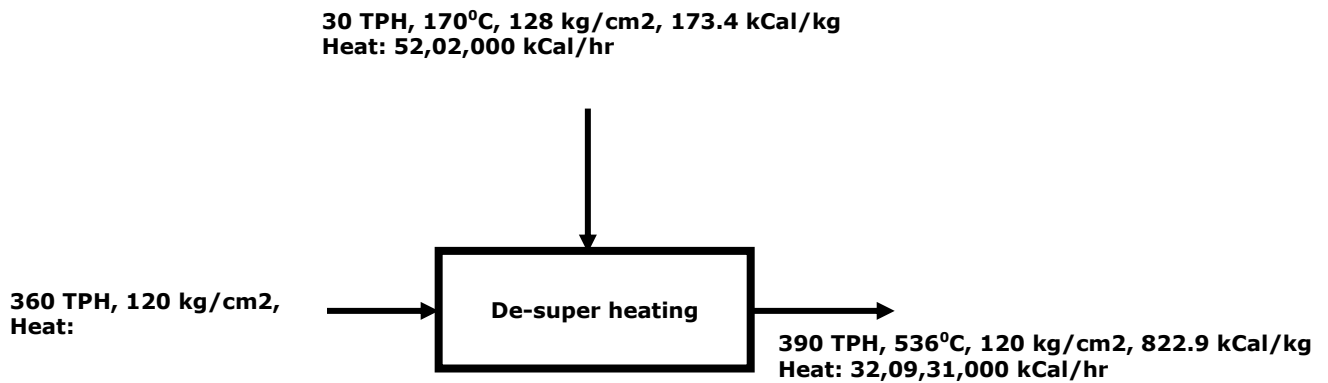
$$= 0.119 \text{ MW power}$$

$$\begin{aligned} \text{Annual savings} &= 119 \text{ kW} \times 7000 \text{ hrs} \times \text{Rs. } 2/\text{unit} \\ &= \text{Rs. } 16.16 \text{ Lakhs} \text{ -----} \rightarrow \mathbf{1} \end{aligned}$$

**Part – 2:**

Enthalpy balance before and after the repairing of soot blowers

Before implementation of project:



Heat available after de-super heating

$$\begin{aligned} &= 390000 \text{ kg/hr} \times 822.9 \text{ kCal/kg} \\ &= 32,09,31,000 \text{ kCal/hr} \end{aligned}$$

$$\begin{aligned} \text{Heat added through water spray} &= 30000 \text{ kg/hr} \times 173.4 \text{ kCal/kg} \\ &= 52,02,000 \text{ kcal/hr} \end{aligned}$$

Therefore, heat available before de-super heating

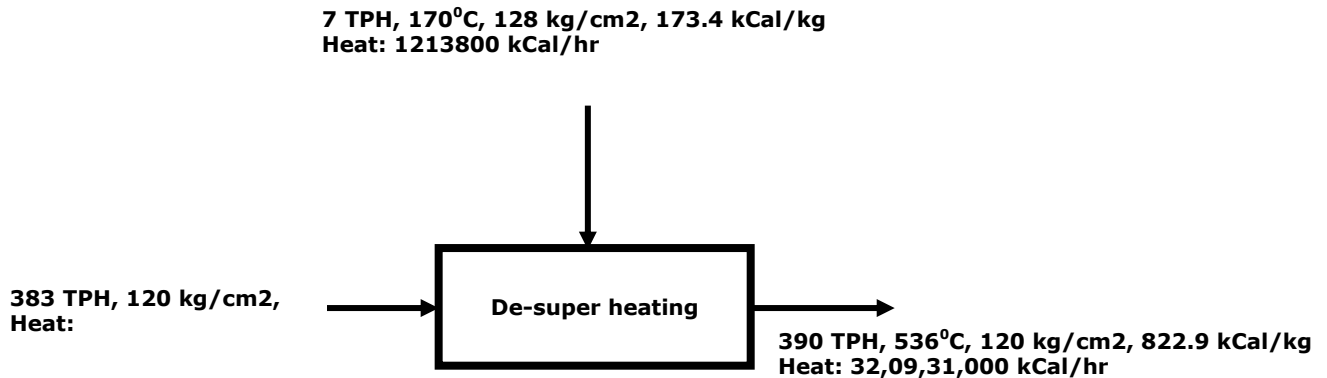
$$\begin{aligned} &= (32,09,31,000 - 52,02,000) \text{ Kcal/hr} \\ &= 31,57,29,000 \text{ kCal/hr} \end{aligned}$$

$$\begin{aligned} \text{Enthalpy of steam} &= \frac{31,57,29,000 \text{ kCal/hr}}{360,000 \text{ kg/hr}} \\ &= 877 \text{ kCal/kg} \end{aligned}$$

Based on the steam tables, steam temperature before de-super heating

$$= 625^{\circ}\text{C}$$

After implementation of project:



After implementing the project, the de-super heating flow reduced from 30 TPH to 7 TPH. To meet the power demand, the main steam flow should be 385 TPH for power generation and 4.584 TPH for soot blowing and 0.416 TPH for extra power generation, total 390 TPH.

However, 7 TPH is adding from water spray, therefore boiler generation is

$$= (390 - 7) \text{ TPH}$$

$$= 383 \text{ TPH.}$$

Heat available after de-super heating

$$= 390000 \text{ kg/hr} \times 822.9 \text{ kCal/kg}$$

$$= 32,09,31,000 \text{ kCal/hr}$$

Heat added through water spray = 7000 kg/hr x 173.4 kCal/kg

$$= 12,13,800 \text{ kcal/hr}$$

Therefore, heat available before de-super heating

$$= (32,09,31,000 - 12,13,800) \text{ Kcal/hr}$$

$$= 31,97,17,200 \text{ kCal/hr}$$

Enthalpy of steam =  $\frac{31,97,17,200 \text{ kCal/hr}}{383,000 \text{ kg/hr}}$

$$= 834.77 \text{ kCal/kg}$$

Based on the steam tables, steam temperature before de-super heating

$$= 555^{\circ}\text{C}$$

Heat savings = (31,97,17,200 - 31,57,29,000) kCal/hr

	=	39,88,200 kCal/hr	
Coal equivalent	=	$\frac{39,88,200 \text{ kCal/hr}}{4600 \text{ kCal/kg}}$	
	=	867 kg/hr	
Annual savings	=	867 kg/hr x Rs. 1.8 / kg x 7000 hrs	
	=	<b>Rs. 109.24 Lakhs</b>	-----→ <b>2</b>
Total savings	=	1 + 2	
	=	Rs. 109.24 Lakhs + Rs. 16.66 Lakhs	
	=	<b>Rs. 125.9 Lakhs</b>	
Investment	=	<b>Rs. 400 Lakhs</b>	
Simple Payback period	=	$\frac{\text{Rs. 400 Lakhs} \times 12 \text{ months}}{\text{Rs. 125.9 Lakhs}}$	
	=	<b>38 Months</b>	

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